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**COAGULANTES À BASE DE PLANTAS PARA TRATAMENTO DE ÁGUAS
RESIDUAIS EM INDÚSTRIAS DE ALIMENTOS**

Campo Grande/2023

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**COAGULANTES À BASE DE PLANTAS PARA TRATAMENTO DE ÁGUAS
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ABSTRACT: Sustainable effluent treatments are essential tools in lowering the environmental impact of industrial activities. The partial or complete replacement of synthetic coagulants by natural coagulants, especially plant-based ones, can reduce the footprint of the effluent treatment due to the higher biodegradability and non-toxicity. Natural coagulants are also generally cheaper. This review focuses on plant-based coagulants used in food industry effluent treatment. Extraction parameters of plant-based coagulants and effluent treatment conditions for different coagulants are presented. Based on an extensive assessment of peer-reviewed papers on food industry effluent treatment, the performance of plant-based coagulants is compared to that of traditional, synthetic coagulants, both alone and as coagulant aids. This review aims to guide researchers and industry professionals in optimizing and scaling up environment-friendlier effluent treatments using natural coagulants.

Keywords: Effluent Treatment; Wastewater Treatment; Coagulation; Natural Coagulants; Sustainability; Biocoagulants.

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1. INTRODUCTION

Industrial activities are one of the leading causes of water pollution due to the generation of significant amounts of effluents that contain toxic species or species that are difficult to degrade [1]. The production of liquid waste by the food industry is sizeable, especially in the animal-based food sector. Slaughtering operations and meat processing generate massive volumes of effluents rich in proteins, organic compounds, and fats [5]. For example, slaughtering a single pig or cow generates 330 L and 700 L of effluents, respectively [2–4]. Although drastically less than the animal sector, the production of plant-derived foods also uses significant amounts of water. For instance, the production of one ton of crude palm oil requires 5–7.5 tons of water [6,7]. Another example is the cassava starch industry, which generates 12–15 L of effluents for each m³ of processed cassava. The effluents from cassava starch production exhibits high biochemical oxygen demand (BOD), chemical oxygen demand (COD), total suspended solids (TSS), total solids (TS), and cyanides [8].

Inadequate disposal of food industry effluents impacts the environment due to the high load of organic matter, heavy metals, alkalinity, and hardness, resulting in water pollution, odor generation, algal blooms, and mortality of aquatic and land animals [4,9]. The appropriate treatment of industrial effluents is carried out by Effluent Treatment Stations (ETSS) [10]. By diminishing the polluting load of effluents, ETSS enable their safe reuse or release into water bodies.

To treat effluents, ETSS utilize coagulation, flocculation, sedimentation, and other physical, chemical, and biological processes [11]. Effluents treatments can be classified into physical (media filtration, settling, adsorption, membrane, and ultraviolet radiation), chemical (electrochemical, coagulation, oxidation, ion exchange, disinfection, catalytic reduction, and softening), and biological (microbial biodegradation, phytoremediation, constructed wetlands, and bioreactor digestion) [12,13]. Among these technologies, coagulation, and flocculation (CF)

are the oldest and most widely employed in effluents treatment due to their simplicity, cost-efficiency, efficacy, and low energy demand [14].

Coagulation involves the addition of a coagulating agent to the effluent to reduce the forces that keep suspended particles apart from colloids. Flocculation agglomerates the resulting material to form larger particles that can be easily separated following sedimentation [13,15]. In effluents processing, CF has been used as a pretreatment to remove suspended impurities and improve the quality of the treated effluent for the subsequent stages [15]. CF operations are also utilized to remove compounds other than suspended particles and colloids, such as pigments, micro-pollutants, organic compounds, oils, and fats [14].

Due to the crucial role of CF in ensuring the safe discharge of effluents, the global coagulant and flocculant market is estimated to reach USD 6.01 billion by 2022, following an annual growth rate of 5.9% between 2017 and 2022 [16]. The economic relevance of CF warrants the study of plant-based coagulants as sustainable substitutes to synthetic-based coagulants [13]. Natural coagulants exhibit greater biodegradability, lower cost, and lesser toxicity and generate less sludge [9,17,18]. Given the alarming amplification of the climate and ecological crises, research applying natural coagulants has critical industrial relevance by promoting more environmentally friendly effluent treatments.

Research on natural coagulants is primarily focused on the treatment of drinking water [19,20]. However, studies that explore the application in industrial effluents, mainly from the food industry, have been growing in recent years. For example, Vieira et al. [9] and Real-Olvera et al. [4] investigated *Moringa oleifera* as plant-based coagulants in the treatment of dairy industry and slaughterhouse effluents, respectively. Vieira et al. [9] reported a 90% removal of color and turbidity, while Real-Olvera et al. [4] obtained a 64% reduction in COD. Dozens of other research studies on the performance of plant-based coagulants to treat food industry effluents will be discussed in the following sections.

This review provides a database for industry professionals and scientists interested in applying plant-based coagulants in food industry effluents treatment.

2. COAGULATION AND FLOCCULATION

As colloidal particles present in effluents exhibit a low sedimentation velocity, ETSs use CF to reduce suspended and dissolved materials [21]. The use of coagulants during CF reduces the turbidity and color of effluents [9]. Turbidity, for instance, is reduced by 85–99% [22]. Coagulation and flocculation agglomerate the impurities from the effluent into larger and heavier particles (called flocs), which can be removed by sedimentation, filtration, or flotation [23] (Figure 1).

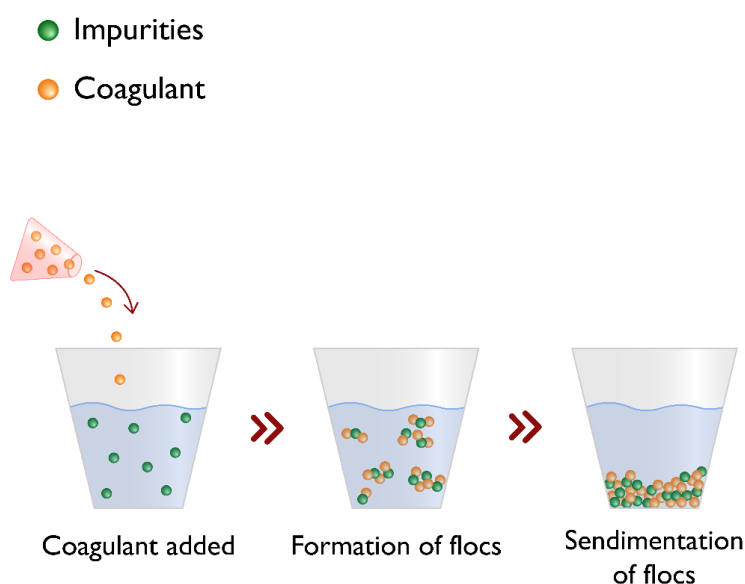


Figure 1 – Representation of the coagulation, flocculation, and sedimentation processes.

Coagulation is a process that affects the physical forces and chemical reactions between the effluent and the dissolved impurities. The coagulating agent generates positively charged ions in the water, which contains negatively charged colloids [21]. As a result, the repulsion

between particles is reduced, causing the particles to collide and stick together to form flocs. From an electrostatic point of view, coagulation reduces the zeta potential (i.e., the electric potential between the liquid medium and the particles' surface) by adding specific ions. According to Okuda et al. [24], the zeta potential is an analytical method to evaluate the effect of coagulation, which helps select the optimal coagulant dosage and medium pH.

According to Pritchard et al. [19], the coagulant must be mixed vigorously for a few seconds immediately after addition into the effluent (Figure 2) to ensure uniform dispersion and high interaction between coagulant and effluent. Coagulation efficiency is a function of the contact between coagulant and suspended particles before the end of the mixing stage. In the subsequent step, flocculation occurs due to the neutralization between the coagulant's acidity and the effluent's alkalinity. Flocs form due to the electrostatic attraction between the positive charges resulting from the ionization of the coagulant and the negative charges of the particles. Flocs are larger, heavier particles exhibiting ionic bonds that tend to precipitate with decreased flow velocity [25].

During flocculation, proper time and stirring must be chosen to ensure floc formation, since the aggregation of suspended particles occurs due to the collision between the particles previously destabilized by the coagulant. Agglomeration is attributed to Van Der Waals forces [26]. The greater the velocity gradient, the faster the rate of particle agglutination. However, the flocs will grow to a maximum limit, as the high shear forces can cause the agglomerated particles to break [21]. As too intense agitation in the flocculation stage can hinder floc stability, lower mixing velocities must be selected at this stage (Figure 2) [27].

Worth noting, when coagulation and flocculation are not carried out properly, the performance of the treatment is compromised, jeopardizing the quality of the treated effluent.

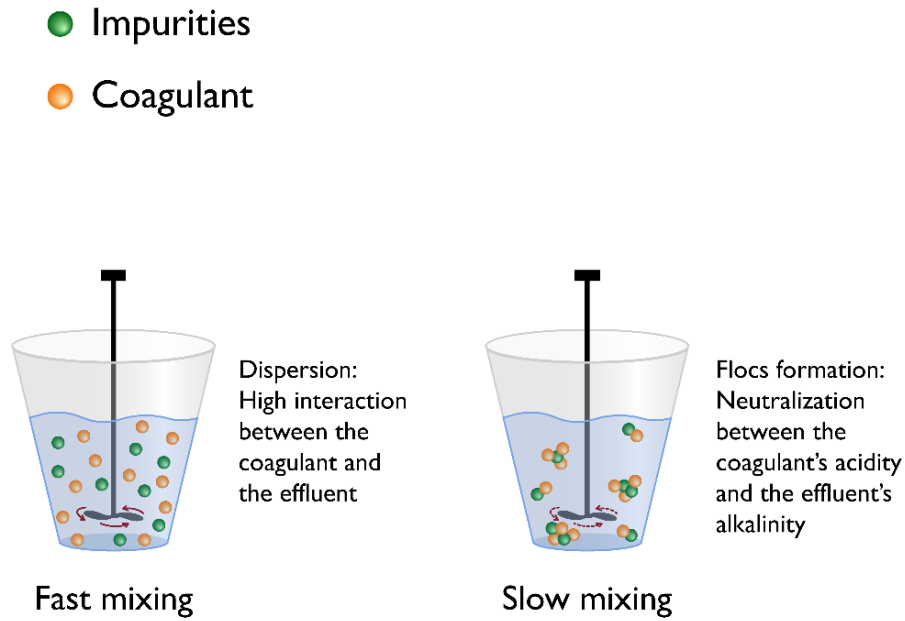


Figure 2 – Representation of the mixing procedure used in the coagulation and flocculation stage.

Table 1 presents the operational conditions (coagulation, flocculation, and sedimentation) used in the treatment of food industry effluents with plant-based coagulants.

Table 1¹ – Operational conditions used in the treatment of food industry effluents with plant-based coagulants.

Due to the wide range of industrial effluents, experiments must be conducted to define the optimal operational conditions for coagulation, flocculation, and sedimentation, aiming at high efficiency and low cost. An efficient way to determine the coagulant dosage and the coagulation pH is to conduct tests in static reactors, known as Jar-Tests (Figure 3). Jar testing entails subjecting the effluent added with specific coagulant dosages to vigorous agitation. The

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stirring rate is then significantly reduced to promote floc formation, and the sample is let to sit for a defined period until the decanted water samples are collected (sedimentation) (Table 1).

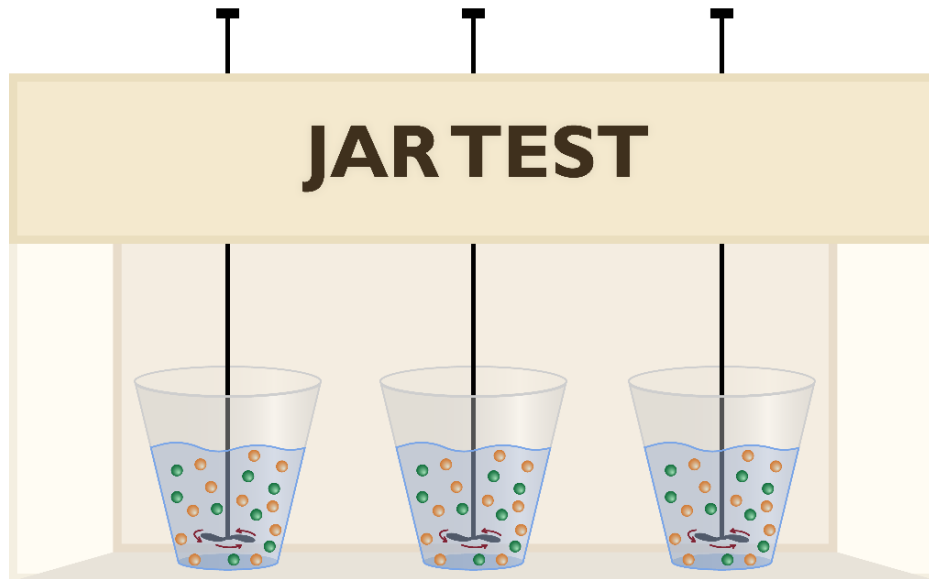


Figure 3 – Representation of a Jar-Test equipment for coagulation, flocculation, and sedimentation tests.

Coagulation efficiency depends not only on the chemical nature of the effluent and the coagulant, but also on such operational conditions as initial pH, coagulant dosage, particle size, temperature, stirring rate, and reaction time [49]. Research on effluent treatment often uses experimental design as a statistical tool to evaluate the ideal conditions in which coagulation, flocculation, and sedimentation occur [6,7,24,34,44]. The resulting data are plotted to illustrate changes in quality parameters (e.g., color, turbidity, COD, total solids, among others) as a function of operational conditions (e.g., medium pH and coagulant dosage). The objective is to derive the optimal conditions for maximum particle removal [50]. Such graphs are of prime importance in the design of Jar-Tests and interpretation of results [51].

3. COAGULANTS

The various coagulants used in effluent treatment can be classified into synthetic coagulants and natural coagulants [9,52]. The coagulant's efficiency depends on the affinity and specificity characteristics, which are a function of its physical-chemical properties [49]. Metal-based materials are the coagulants traditionally used in effluents treatment. Despite the broad applicability of metal-based coagulants, the challenges associated with their use have prompted research efforts to develop environment-friendly biobased coagulants [14].

3.1. SYNTHETIC COAGULANTS

The most used synthetic coagulants are trivalent iron and aluminum salts, with AlCl_3 , $\text{Al}_2(\text{SO}_4)_3$, FeCl_3 , and $\text{Fe}_2(\text{SO}_4)_3$ being the most frequent due to the low cost and proven coagulant capacity [53,54]. The choice depends primarily on the effluent's characteristics.

Coagulation performed with aluminum and iron salts involves chemical and physical phenomena. The hydrolysis promoted by the coagulant forming hydrolyzed and positive-charged species is a chemical process. The formation of hydrolyzed species depends on the coagulant dosage and the effluent's pH [55]. In general, these coagulants will only be effective if the effluent is alkaline; otherwise, coagulation will be limited due to excess protons released by the coagulant. In turn, the physical mechanisms encompass the contact of the hydrolyzed species with the impurities present in the effluent, forming flocs (flocculation stage) [21]. Particle aggregation results from the neutralization of negative charges of the effluent's solids by the hydrolyzed species, ensuring floc growth and hence rapid precipitation [55].

Despite the recognized efficacy of synthetic coagulants in effluents treatment, the use of agents based on aluminum salts requires strict control over the residual concentration of synthetic material in the treated effluent. According to Yin [23], after the salt is solubilized, the

cation released will be adsorbed onto the solid suspended material. In other words, the sedimented material will have a high concentration of the cation (for example, Al^{3+}), which impedes the safe discharge of the treated effluent in the environment. Studies link high aluminum intake to potential health conditions, such as Alzheimer's disease [13].

3.2. NATURAL PLANT-BASED COAGULANTS

Plant-based coagulants play a prominent role in sustainable effluents treatment due to their high biodegradability, non-corrosive nature, and non-toxicity. An increasing number of research papers focus on the coagulation properties of seeds and bark resins from different plant species, but also of bone shell extracts, extracts from shellfish exoskeleton, and natural mineral soils [14,20,56,57].

Natural coagulants are composed of large molecular chains, either positively or negatively charged. These coagulants can be cationic, anionic, or non-ionic, with the former two collectively termed polyelectrolytes [58]. However, only cationic polyelectrolytes (those with positive charges) are ideal for use as coagulants [14].

Coagulants characterized as cationic polyelectrolytes are ideal in effluents treatment because the colloidal material present in the effluent generally exhibits a negative surface electrical charge. Cationic polyelectrolytes produce cationic species in the effluent, destabilizing the particles and thus contributing to coagulation. The resulting attraction between particles (Van der Waals force) enhances floc formation due to a reduction in the negative charge of the colloidal surface [52-54].

Natural coagulants have been studied as partial or total substitutes of synthetic coagulants to improve the CF stage – both the quality of the flocs produced and the reduction/elimination of metals in the final sludge [52]. The use of natural coagulants combines the properties expected for effluent treatment with abundant availability, low toxicity and cost,

high biodegradability, and low rate of waste sludge production [52,59,60]. Nevertheless, the presence of natural organic polyelectrolytes in drinking water treatment can increase the organic matter content, prompting the onset of unpleasant tastes and odors. Therefore, the introduction of natural coagulants in water treatment must be carefully considered, as the treated water is likely to contain residues that will be ingested by consumers [19,20,56]. In effluent treatment, this aspect is still little explored [61-63].

Table 2 presents the main conclusions of several studies on plant-based coagulants in the treatment of food industry effluents.

Table 2² – Plant-based coagulants used to treat food industry effluents.

3.2.1 Parameters that influence the performance of plant-based coagulants

In view of the wide range of existing coagulants (both synthetic and natural), choosing the most efficient can be challenging. The process parameters (such as dosage, settling time, mixtures, temperature and pH) must be weighted appropriately to obtain the best performance in removing contaminants [64,65]. Tables 1 and 2 summarize the process parameters commonly used in food industry effluents treated with plant-based coagulants, as well as the main performance results.

Dosage

Inadequate coagulant dosing results in unsatisfactory water quality after treatment. Therefore, it is critical to determine the dosage range needed to obtain maximum pollutant removals at minimum cost. Among different coagulation mechanisms, only charge neutralization

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and bridging are negatively affected by dosage, mainly due to the stoichiometric relationship [44,66].

When the effluent's turbidity is high (>100 NTU), the required coagulant dosage tends to be lower compared to low turbidity effluents (5–10 NTU) [59]. A likely cause is the collision frequency between particles and coagulant [15]. As high turbidity means a high concentration of impurities (and a high collision frequency), coagulation is more likely. In this case, lower dosages of coagulant are necessary. In contrast, low turbidity requires a high dosage of coagulant because the collision frequency between impurities and coagulants is lower [50]. Optimal dosage can be obtained by plotting the measured turbidity (or any other pollutant parameter) versus the applied dosage [60,61].

There is a decline in contaminant removal efficiency when the coagulant dosage is less than or exceeds the required dosage. Overdosing can lead to charge reversal and consequently result in particle repulsion, preventing floc formation. Overdosing restricts the number of available adsorption sites by covering the coagulant surface [44,51]. Therefore, adding more coagulant to the effluents treatment does not enhance the coagulation process. On the other hand, a dosage much lower than necessary results in incomplete and ineffective coagulation because most of the particles remain in suspension.

Real-Olvera et al. [4] tested a dosage of 3 to 7 g/L of *Moringa oleifera* for the treatment of slaughterhouse effluent and observed that 7 g/L yielded the best results. When *Cassia obtusifolia* at a dosage of 0 to 2.5 g/L was used in effluent coagulation, the optimal condition was 1.0 g/L to treat palm oil residue [6] and 2 g/L for rice starch [62].

pH

A solution's pH affects the efficiency of the coagulation process by changing the electrochemical nature of the solvent and ionic polymers used [44,63]. Therefore, the system's

pH optimization is essential to ensure efficient coagulation [61,66]. The decrease in pH lowers the load of natural organic matter (NOM), reducing their water solubility. Consequently, coagulation efficiency is reduced, as the main coagulation mechanism is charge neutralization, in which cations or polyelectrolytes are required to bind to the negative charge of the NOM [44,61]. An optimal pH is also critical for forming metal poly-hydroxides and the precipitation of solid colloidal phases [61]. Cationic polyelectrolytes are the most widely used organic polyelectrolytes owing to their ability to bind with negatively charged NOMs. The positive charge in these polymers can increase at lower pH when the functional groups responsible for the cationic behavior are amines (primary, secondary, and tertiary) [61].

Some studies have optimized the pH of the treatment system when using plant-based coagulants, for example *Coccinia indica* [67], okra gum [68], cactus, and hyacinth bean peels [69]. The optimal pH for coagulation using okra gum was 9.2, with 98.3% SS removal [68]. At this pH, okra gum uncoiled further to achieve a flat, dangling form, which enhances the coagulation process. Most legumes used as natural coagulants perform better when coagulation occurs at an optimized pH of 7 to 8.5 [20,56]. However, the same coagulant can exhibit different optimal pHs depending on the effluent under treatment. For example, *Moringa oleifera* showed optimal performance at pH 9.0 for slaughterhouse effluent [4]; between 4.0 and 5.0 for the effluent from the pulp of coffee fruits [6], and 4.0 for distillery spent wash [46].

Temperature

Temperature is the factor that receives the least attention in effluent treatment. Few studies have reported the effect of temperature on treatment efficiency [6,36,40,70]. Temperature affects coagulation kinetics and impurity removal efficiency [71,72]. Coagulation efficiency improves with an increase in temperature due to the higher collision rate among particles. This

results in lower viscosity, favoring the homogeneous dissipation of the coagulation species in the mixing stage [73].

At low temperatures, flocc aggregation tends to be weak due to the lesser particle-particle collisions. Due to the formation of irregular flocs under low-temperature conditions, the coagulant dosage required to remove organic matter is higher [70,72].

In many cases, the effluent's temperature is a non-controllable parameter, which affects the removal of NOM by coagulation. Therefore, dosages must be reassessed across seasons to account for temperature changes [2,70].

For plant-based coagulants, the optimal process temperature is 25-30°C [6,36,40,70]. As the active agents in plant-based coagulants are generally proteins, system temperature must be increased carefully to avoid a reduction in the coagulation capacity due to protein denaturation. As denaturation causes changes in the protein's spatial configuration, its biological activity is reduced or lost.

Mixing

Mixing is crucial in coagulation processes, including both rapid mixing to promote the interaction of coagulants with suspended particles to form microflocs, and slow mixing to promote microfloc aggregation and large floc formation. Excessively low mixing speed and considerably short mixing time can decrease the rate of floc formation, while excessively fast mixing speed and considerably long mixing time can break the flocs, yielding poor settling efficiency [55,70,71]. As shown in Table 1, mixing parameters in the treatment of food industry effluents with plant-based coagulants vary from 100 to 300 rpm for 30 s to 5 min for fast mixing, and 20 to 100 rpm per 5-40 min for fast mixing, followed by sedimentation for 30 min to 24 h.

3.3 PLANT-BASED VERSUS SYNTHETIC COAGULANTS

In effluent treatment, the coagulation stage is conducted by adding a coagulating agent to reduce or remove suspended impurities and other types of pollutants, such as organic compounds [15,74]. The coagulating agent can be synthetic-based or naturally derived [75].

Currently, synthetic coagulants predominate in industrial settings due to their low cost, high efficiency, easy handling, and widespread market availability. AlCl_3 , $\text{Al}_2(\text{SO}_4)_3$, FeCl_3 , and $\text{Fe}_2(\text{SO}_4)_3$ are the most used coagulants [76]. Although these factors drive the choice of synthetic coagulants over plant-based alternatives, synthetic agents have raised controversial issues due to their low biodegradability and toxicity to living organisms. Residual aluminum concentrations are still detected after treatment [76,77]. Researchers warn that Alzheimer's disease is linked to aluminum neurotoxicity [78]. Furthermore, synthetic coagulants can form dangerous by-products such as acrylamide, a carcinogen and neurotoxic substance [79]. According to Kurniawan et al. [79], the disposal of toxic sludge pollutes water and soil, affecting plant and animal species negatively. As a result, synthetic coagulants are not considered sustainable and do not qualify as green options [76]. Therefore, it is necessary to promote sustainable and equally efficient coagulating agents.

Natural coagulants are biodegradable, non-toxic, non-corrosive, reduce the amount of sludge, and are environmentally friendly [9,17,18,37]. Natural coagulants are recognized in traditional water purification, especially in impoverished communities [20,56]. Based on these applications, natural coagulants have attracted the scientific community's attention due to their significant health and environmental benefits, and their efficiency in removing contaminants.

Several studies have proven the effectiveness of plant-based coagulants in effluents treatment applications: removal of 98% of color and turbidity from dairy industry effluents [9]; 64% COD removal from slaughterhouse effluents [4]; removal of 87% TSS and 55% COD from palm oil milling effluent [6]; reduction of 54% TSS, 100% COD, and 100% nitrate and nitrite

from coffee fermentation effluents [44]; reduction of 95% suspended solids and 52.2% COD from palm oil milling effluent [35]; removal of 96.5% color, 87% COD, and 99.9% turbidity from distillery spent wash [46]; and removal of 90% of COD from palm oil milling effluent [39]. However, these studies are massively small-scale. The industrial application of natural coagulants in effluents treatment is still limited, especially owing to a lacking tax incentive and inconsistent information on performance, quality control, and production standards of plant extracts [20,76,80].

Although *Moringa oleifera* is the most commonly used and extensively researched plant-based coagulant [4,29,47,50,75], several others have been identified, such as: Nirmali seeds (*Strychnos potatorum*) [81]; Dolichos lablab or hyacinth bean (*Lablab purpureus*) [69], banana (*Musa paradisiaca*) [82]; Roselle seeds (*Hibiscus sabdariffa*) [83,84]; cactus species [85]; watermelon seeds [86]; sicklepod (*Cassia obtusifolia*) [6,7]; rice starch [37,38]; okra (*Abelmoschus esculentus*), sandpaper tree (*Ficus exasperate*), and *Bridelia ferrugineae* [41].

3.4. ASSOCIATION BETWEEN NATURAL AND SYNTHETIC COAGULANTS

Despite the environmental benefits of using natural coagulants in drinking water and effluents treatment, these might not be as effective as synthetic coagulants. To harness the advantages of natural coagulants without hindering the treatment efficiency, they can be combined with synthetic coagulants either as a composite coagulant or as coagulant aid [87,88]. The former is produced by combining two types of coagulants as a single coagulant, while coagulant aids are materials added some time after the dosing of the primary coagulant. These approaches minimize the consumption of non-renewable coagulants and their associated environmental impact [89].

There are few studies on the association of natural coagulants with synthetic coagulants, such as ferric chloride, polyaluminum chloride, and aluminum sulfate [62]. Shak and Wu [7]

reported a 55% reduction in alum when gum extracted from *Cassia obtusifolia* seeds was employed as a coagulant aid. More impurities were adsorbed onto the coagulant aid due to the polymeric structure of the natural gum.

Ghebremichael et al. [90] concluded that dosing the moringa coagulant prior to alum resulted in better removal of turbidity and dissolved organic carbon from surface water (river). Furthermore, the use of the natural coagulant aid reduced the alum dosage by 50-75%. Similar benefits were achieved by dosing alum and moringa coagulants together in concrete effluents treatment [75]. Freitas et al. [91] also highlighted that dosing the moringa coagulant after alum results in greater turbidity removal than dosing them together to treat polluted stream water.

Natural materials that might not perform well as coagulants individually (e.g., lignin, starch, green algae, and cactus mucilage) can be used as coagulant aids or as part of a composite coagulant [13,89,91,92]. These coagulant aids strengthen the flocs through charge neutralization and bonding with the flocs formed by the primary coagulant. As the treatment becomes more effective and the dosage of the primary coagulant is reduced, the residual synthetic coagulant (e.g., aluminum) is also minimized.

4. ACTIVE PRINCIPLE UNDERLYING COAGULATION WITH NATURAL AGENTS

In broad terms, most natural coagulants can be categorized into two groups based on the main compounds with coagulation activity: polysaccharides and proteins. Examples of the first group are plant- or animal-derived materials such as chitosan, starch, and mucilage, while protein-based natural coagulants typically originate from plants [9,93]. The presence of hydroxyl and amino functional groups in these compounds contribute to their coagulation capacity [13].

Plant-based natural coagulants are mostly water-soluble organic molecules [94-96] extracted primarily from seeds [97,99] and mucilages [100,101]. For example, *Moringa oleifera* seeds are used as a coagulant due to the presence of soluble cationic proteins capable of reducing

the turbidity of the treated liquid [4,102]. Nordmark et al. [103] isolated eight different cationic protein fractions from aqueous extracts of moringa seeds. In turn, Kwaambwa and Maikokera [104] hypothesized that the active agents responsible for coagulation in moringa are dimeric cationic proteins with a molecular mass in the range of 12–14 kDa and an isoelectric point of pH 10–11, which indicates a highly cationic nature.

Ghebremichael et al. [90] concluded that the active compound in moringa is not a single protein, but rather a mixture of proteins with similar physical characteristics. According to the authors, this protein mixture is heat-resistant and exhibits clotting activity after 5 h of heat treatment at 95°C. This property renders the active ingredient ideal for use in water and effluent treatment systems exposed to high temperatures (35-40°C), as frequently found in tropical countries.

Unlike conventional metallic synthetic coagulants, natural coagulants exhibit particularities that affect the quality control of the active ingredient, rendering it more challenging. This behavior results from the extraction method (which comprises various stages) and the coagulant source – especially plant-based coagulants, where the compounds vary according to the plant species and growth conditions [13].

Worth noting, non-coagulating impurities will inevitably be present in extracted natural coagulants if further purification is not conducted. The presence of impurities that possess no coagulation capacity affects the coagulation efficiency [102]. For example, the lipid fraction may inhibit the contact between coagulant and impurities, rendering the floc formation ineffective, while carbohydrates may increase the organic matter concentration in the solution [102,105]. Extensive purification can be conducted but will incur additional costs. According to the source and extraction approach, the variable performance of natural coagulants might hinder quality control [13].

5. PROCESSING TECHNIQUES OF NATURAL COAGULANTS

Whenever the objective is to utilize the isolated active ingredient (e.g., a particular protein), coagulant preparation must follow three main stages (Figure 4): a) primary – flour preparation; b) secondary – protein extraction; and c) tertiary – purification [18]. The characteristics of the coagulant and its performance in CF are directly influenced by the order of these stages [106].

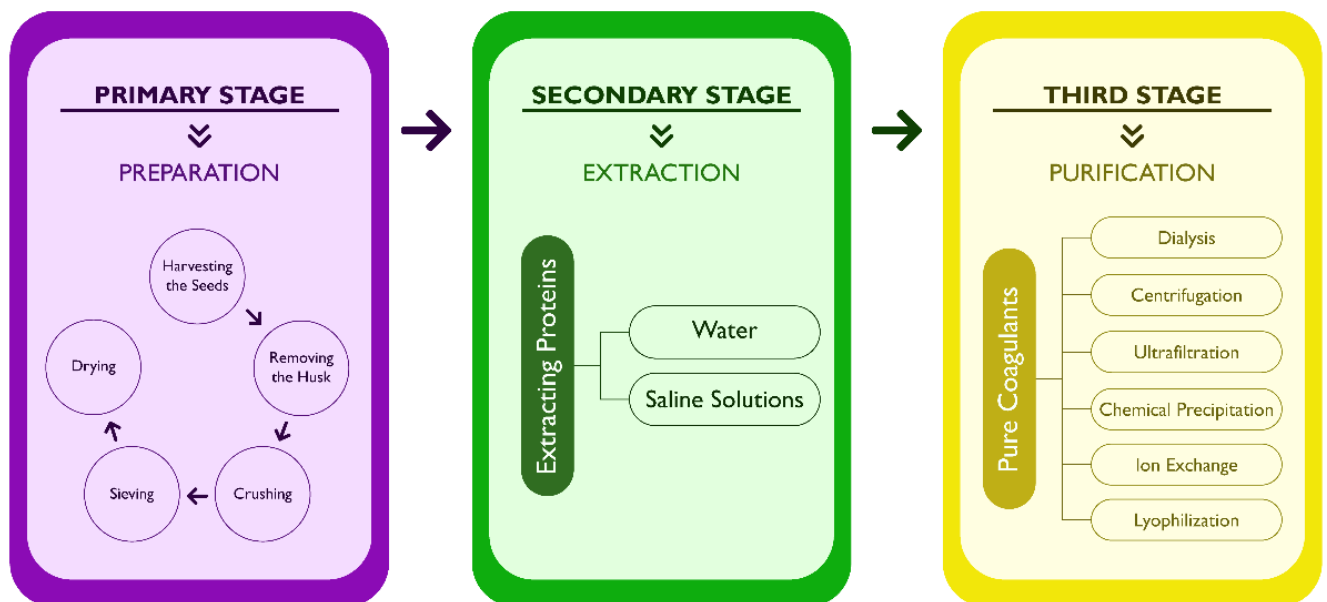


Figure 4 – Diagram of the main processing techniques of natural coagulants.

Using *Moringa oleifera* as a reference, the primary stage includes harvesting the seeds, removing the husk, crushing, sieving, and drying. The recommended particle size for water and effluent treatment varies between 0.25 mm and 1.25 mm [107]. Moringa seeds contain a wide variety of undesirable compounds in CF that increase the organic load in the treated effluents. Therefore, the material obtained in the primary stage is further treated.

The secondary stage consists of extracting proteins with water or saline solutions [18]. The simplest extraction method uses clean water. Jung et al. [108] mixed powdered moringa

seeds with water and stirred the mixture to release the coagulating compounds, which are positively charged proteins. However, the coagulation efficiency of this extraction approach is often unsatisfactory due to the presence of non-coagulating impurities and a low number of coagulating compounds [13]. The main disadvantage of water extraction is the increased COD due to the dissolved organic carbon content, which discourages the use in drinking water treatment [109]. In effluents treatment, this method's efficiency is controversial: COD dropped in some studies and increased in others [33].

In the study by Oladoja [14], salt solution extraction exhibited better coagulant capacity than water extraction, which can be explained by the higher number of soluble proteins present in salt extracts. The author recommends using moringa seeds as a coagulant in the treatment of drinking water and wastewater effluents intended for water reuse only after purifying the active proteins.

The coagulation capacity of a particular substance can be improved by using salt solutions (e.g., NaCl and CaCl₂) during extraction [110,111]. The use of saline solution enhances protein extraction from natural coagulants due to the salt's capabilities of promoting protein-protein dissociation and increasing the solubility of proteins, which increases the efficiency of the coagulant ion [111]. Megersa et al. [111] demonstrated that the addition of salt solutions (NaCl, KNO₃, and NH₄Cl) enhances the coagulation performance compared to the water-extracted moringa coagulant. The optimum coagulant dosage extracted using 0.5 M NaCl was 2 mg/mL, yielding a 91% turbidity removal. Such improvement is attributed to the increased solubility of proteins from the natural coagulant in the presence of salt due to the breaking down of protein-protein bonds. Carvalho et al. [110] reported that moringa coagulant extracted with CaCl₂ resulted in higher turbidity removal compared to NaCl extraction, which could be explained by the participation of calcium ions in the coagulation process.

Apart from increasing the extraction yield (i.e., number of compounds with coagulation capacity), the purity of natural coagulants can be improved to reduce impurity concentration and

coagulant dosage. Organic compounds present in natural coagulants that do not take part in coagulation will possibly end up in the treated water as dissolved organic matter [112]. The presence of organic residues is undesirable due to the increased risk of bacterial growth, which can serve as a substrate for the formation of hazardous by-products [113,114]. To avoid such adverse effects, natural coagulants must be purified after extraction.

Only those compounds that contribute to the coagulation properties are purified in the third stage. Regardless of the plant source, coagulating compounds are either polysaccharides or proteins [13]. To obtain pure coagulants, purification can be carried out using a combination of different methods, such as dialysis, centrifugation, ultrafiltration, chemical precipitation, ion exchange, and lyophilization [18,24]. The final extract may differ based on the purification method, and different solvent extractions and extract fractionation will yield different types of products [115].

Sánchez-Martín et al. [112] investigated the impact of ion exchange purification using NaCl solution on the coagulation performance of moringa extract. The optimum dosage of the single-step purified coagulant (elution with 0.6 M NaCl) was two times higher than the two-step purified coagulant (first elution with 0.3 M NaCl followed by a second elution with 0.6 M NaCl) in terms of turbidity removal. This led to the production of more purified coagulants containing active coagulant proteins after the second elution.

The purified coagulant produced via ion exchange performed at par with the conventional alum coagulant in terms of required dosage (1 mg/L) and turbidity removal efficiency (83%) for natural river water [111]. Without further purification, the moringa extract could only achieve 50% turbidity removal at a similar dosage and required fourfold the dosage for 83% removal efficiency. Therefore, the purification process can produce natural coagulants with a higher proportion of active coagulation compounds, which results in better performance even at lower optimal dosage [13].

Due to the high cost of ion-exchange chromatography, researchers have sought alternative purification approaches that are more economically viable at the industrial level [13]. Relatively simple chemical precipitation (using ammonium sulphate) of compounds possessing coagulation activity has been proposed for the purification of moringa extract [95,116]. Choudhary and Neogi [116] reported that the natural moringa extract isolated with saturated ammonium sulphate exhibited superior turbidity removal efficiency than alum. Hence, a simple but effective isolation and purification method for natural moringa extract may result in a natural coagulant with satisfactory coagulation capacity [13].

The methodology involved in the production of moringa coagulant can be replicated to extract and purify natural coagulants from other plant sources – e.g., seeds of plantago (*Plantago major L.*), beans (*Phaseolus vulgaris*), chestnut (*Bertholletia excelsa*), basil (*Ocimum basilicum*), oak (*Quercus robur*), hibiscus flower (*Hibiscus L.*), or cactus pads from *Opuntia* species [83,93,117-120]. In general, the extraction and purification of plant-based natural coagulants rely on three stages, as shown in Figure 3. Table 3 presents the manufacturing process of natural coagulants used to treat food industry effluents.

Table 3³ – Natural coagulants used in the treatment of food industry effluents.

6. MECHANISMS OF COAGULATION WITH NATURAL AGENTS

Natural coagulants can be obtained from plants, animals, and microorganisms. The main mechanisms involved in the coagulation with plant-based coagulants are adsorption and charge neutralization or alternatively adsorption and bond formation. It is difficult to define the exact mechanism because the phenomena can co-occur [121,122]. Adsorption and charge neutralization refer to the sorption of two particulates with oppositely charged ions, while

³ attached

interparticle bridging occurs when a coagulant provides a polymeric chain that sorbs particulates [101]. These two mechanisms are involved in the coagulant properties of plant-based coagulants [58,101].

Amran et al. [123] discuss in more detail how plant-based coagulants promote the coagulation of pollutants in effluents. In charge neutralization, an ionizable polymer (present in the coagulant) stabilizes the colloidal particles, which otherwise would repel one another for being negatively charged. In polymer adsorption, long-chain polymers partially attach themselves to the surface of the colloidal particles due to the affinity between them. The unattached parts, composed of loops and tails, are the main structure involved in bond formation or polymer bridging. Bridging ensures the formation of pollutant flocs by decreasing interparticle repulsion. Sufficient coagulant dosages will provide the required amount of polymer to promote strong polymer bridging.

In the study by Vieira et al. [9], the sorption potential of moringa coagulant was assessed for color, turbidity, and COD removal in dairy industry effluents (DIE). Maximum adsorption of DIW components from aqueous solutions occurred using 1 g/L of moringa seeds with a 60 min agitation time, which suggested an excellent affinity between DIE components and sorbent. Furthermore, the moringa coagulant showed sorption capacity within a pH range from 5 to 8.

Real-Olvera et al. [4] investigated the adsorption of organic pollutants from slaughterhouse effluents when *M. oleifera* was employed as a natural coagulant. The results indicated that 180 min is necessary for high adsorption. The maximum adsorption capacity of 0.523 g COD/g powder suggests a good affinity between organic pollutants and powdered seeds. Moringa seed powder exhibited sorption capacity over the pH range 5 to 9, but the best results were obtained at high pH levels.

7. BENEFITS OF USING NATURAL COAGULANTS

Natural coagulants overperform synthetic coagulants in terms of biodegradability, non-corrosivity, and lower or non-toxicity [24,54,106] (Figure 5). Such features are attractive for the development of “greener” water and effluents treatment, where processing costs are reduced while color and turbidity removal are improved [122]. In addition, the sludge produced during the coagulation process is innocuous and has a volume 4–5 times smaller than the sludge produced when aluminum sulfate or ferric chloride are used [9,124]. Furthermore, natural coagulants do not significantly change the pH of the medium [124] and do not cause corrosion problems [99].

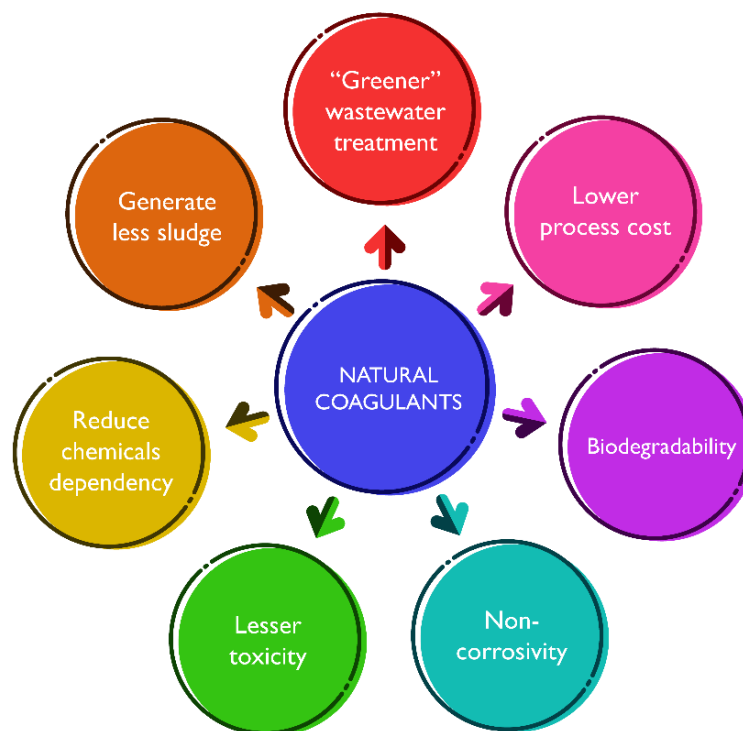


Figure 5 – Advantages of natural coagulants over synthetic coagulants.

Although efficiency is one of the most critical factors in water and effluents treatment, other criteria are equally relevant for the long-term reliability of sustainable, plant-based

coagulants. In effluent treatment, sustainability encompasses the integration of environmental, social, economic, and technical aspects [125] (Figure 6).

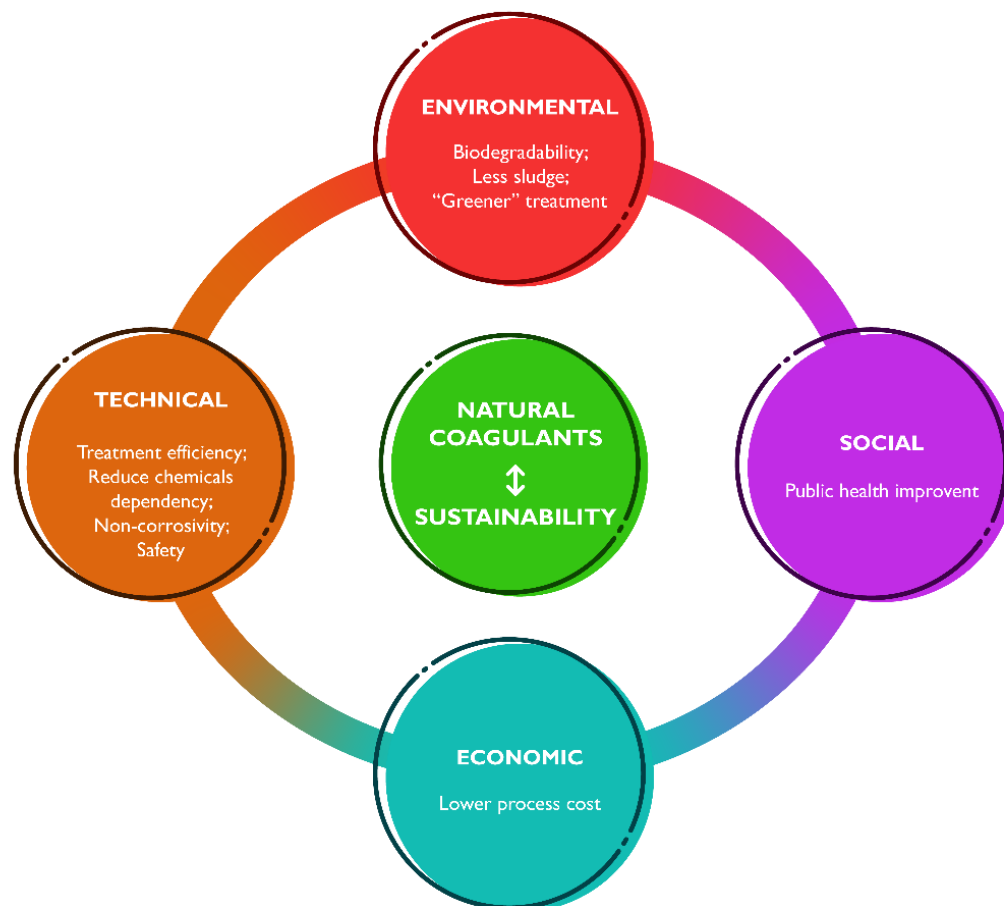


Figure 6 – Relevant sustainability criteria in effluent treatment.

8. ECONOMIC ASPECTS OF PLANT-BASED COAGULANTS

Synthetic coagulants are predominant in effluents treatment because of their low cost, easy handling, high availability, and market diversification. Nonetheless, synthetic coagulants do not fit into green chemistry due to the residual aluminum concentrations found after treatment [76,126].

Plant-based coagulants become economically attractive when such advantages as biodegradability, non-toxicity, non-corrosiveness, and easy implementation are factored in [127].

In addition, plant-based coagulants reduce the volume of sludge produced as well as handling and treatment costs due to the biodegradable nature of water treatment residuals [76]. According to Othmani et al. [128], effluents treatment systems will eventually replace synthetic coagulants with plant-based alternatives given their low price, multipurpose application, biodegradability, and abundant sources.

In a world facing a climate emergency, the depletion of natural resources, and widespread environmental degradation, plant-based coagulants are in line with global initiatives for sustainable development [62]. The necessary advance of environmentally sustainable technologies will contribute to the broader use of plant-sourced coagulants, reducing production costs due to economies of scale. Moreover, plant-based coagulants will become ever more competitive as the high performance in effluents treatment demonstrated in the scientific literature is translated into industrial practice [23].

Contrary to the abundant studies on the efficiency of plant-based coagulants to treat effluents (especially from the food industry), direct comparisons of production costs and end prices between natural-origin and synthetic coagulants are incredibly scarce. According to Vijayaraghavan et al. [62] and Yin [23], the attractive price of *M. oleifera* coagulant compared to other natural coagulants is the result of the plant's widely publicized advantages and the coagulant's broad application across different effluent treatment systems.

A single *M. oleifera* tree produces approximately 2,000 seeds per year. This amount can treat 6,000 L of water at a dosage of 50 mg/L [18]. If fully grown, the yield of a single tree can increase by up to 20,000 seeds, which would be enough to treat 60,000 L of water per year [18]. A study by the Water and Environmental Health at London and Loughborough (WELL) [129] shows that an *M. oleifera* tree producing an average of 3 kg of seeds can treat 30,000 L of effluent at a dose of 100 mg/ L. In about 1 ha, it would be possible to harvest 3,000 kg of seeds, which would be able to treat 30,000 m³ of water [18].

The production costs of moringa seed depend on several factors, including harvest yield, climate, and agricultural practices. For perspective, the purchase price of moringa seed in Malawi was £7.5 per 1000 m³ of treated water in 1994, while the cost of alum and soda ash was £49.8 [130]. In Malaysia, however, the production cost of 1 kg of *M. oleifera* in 2006 was approximately US\$2, twice that of alum [59].

The main elements hindering the pricing and commercialization of plant-based coagulants include: (a) insufficient plantations to allow bulk processing of the source plants; (b) seasonal variations of the raw material; (c) little market demand; (d) incipient specialized knowledge and research development on economically viable extraction methods, storage and preservation conditions, and optimal effluents treatment parameters; (e) currently limited industrial use; (f) shortfall of market awareness and interest; (g) well-established and competitive market focused on synthetic coagulants; and (h) absence of production regulation and quality control for plant extracts [13,20,76,80].

While the cost-effectiveness of plant-based coagulants is currently restricted to small-scale use and academic research, exploration can be widened upon stakeholder endorsement [18,62]. Governmental and non-governmental regulatory bodies should implement environmental rules that encourage industries to use natural coagulants, including reduced tax payments and facilitated loans to subsidize implementation costs [77,80]. Furthermore, research should be advanced to identify the best natural coagulants with economic and industrial potential [76].

9. RECENT ADVANCES AND FUTURE PERSPECTIVES FOR PLANT-BASED COAGULANTS IN WATER TREATMENT

Plants with coagulation capacity in addition to Moringa oleifera

Othmani et al. [128] evaluated the performance of moringa, cactus, okra, and mango in freshwater and effluents remediation. According to the researchers, not only do the selected plants belong to different families, but also their coagulant capacity depends on the parts from which the coagulant agents are extracted. The parts of interest are seeds for moringa and mango, seed pods for okra, and pad for cactus. The coagulant capacity of these materials depends on the active agent extracted (polysaccharides, proteins, or both), which produces a variation in the removal rate of contaminants among plants.

Thakur and Choubey [131] observed an 80.7% turbidity reduction when treating synthetic cloudy water with moringa. When using okra, the removal rate was 78.7%. Kazi and Virupakshi [132] demonstrated that moringa seed reduced 82% and 83% of turbidity and COD, respectively, of tannery effluent, while cactus mucilage exhibited removal percentages of 78.5% and 80.6% for turbidity and COD, respectively. Qureshi et al. [133] reported that mango provided a 98% turbidity reduction versus 86% for moringa. In their study, Othmani et al. [128] found that the sequence mango > moringa > cactus = okra defines the plants' ability to remove turbidity. Given these results, mango should be further investigated for its coagulation capacity. In addition, active agents should be better explored. Although previous studies claim that proteins are the only active coagulant compound in plants, Seghosime et al. [134] hypothesize that the high carbohydrate content (76.73%) in mango seeds contributes to the plants' coagulant activity.

Therefore, the valorization and research of biomaterials for water and effluent remediation can be considered a gateway to applying green chemistry and clean technology in treatment systems [128].

Integrated process

An integrated process is a strategy to enhance the use of natural coagulants by combining coagulants with other treatment technologies. The treatment goals are met by utilizing the strength of each process while minimizing their shortcomings [13]. An example is integrating a coagulation stage (with natural coagulants) with a biological treatment. Hameed et al. [135] implemented a coagulation step (with a tannin-based coagulant) before the biological treatment. The integration reduced the organic load content, generating savings due to the lower need for aeration. Pavón-Silva et al. [136] demonstrated that combining coagulation and biological treatment resulted in COD removal rates of up to 99% in the treatment of food industry effluents. These results indicate that natural coagulants improve the performance of the subsequent treatment steps.

Another example is integrating coagulation with membrane systems, where the tendency towards membrane fouling is minimized [15]. Chitosan, utilized as a natural coagulant, improved nanofiltration membrane fouling in relation to organic matter by neutralizing the charges and weakening the antifouling capability (electrostatic repulsion) of the membrane [12]. Furthermore, integrating coagulation with electrolysis further refined the quality of the supernatant (by degrading the organic compounds in the effluent), making it suitable for discharge into water bodies [13]. Integrated processes involving coagulation and other treatments improve the quality of the treated effluent, allowing its safe disposal. Natural coagulants can be used in pre- or post-treatments combined with other technologies to benefit the entire process [13].

Improved extraction and purification of natural coagulants

Unlike synthetic coagulants, where quality characteristics are precisely controlled, the quality control of natural coagulants is challenging. Such peculiarity is associated with the synthesis of coagulants, which can be obtained through various processes and sources. To

overcome this disadvantage and produce a pure natural coagulant, it is necessary to optimize the extraction process. The simplest extraction method uses water. However, the efficiency of this approach is usually unsatisfactory. This can be circumvented by optimizing the extraction method and including a purification step.

The coagulation capacity can be increased by using saline solutions (e.g., NaCl and CaCl_2) during the extraction step [110,111]. Megersa et al. [111] found that the use of saline solutions (NaCl, KNO_3 and NH_4Cl) increased the turbidity removal efficiency of moringa from 37% using water extraction to 91%. This result can be explained by the Debye-Huckel theory (increasing solvating power) [13]. Salts increase protein solubility by breaking down the protein-protein bonds of natural coagulants [111]. The number of active compounds with coagulation capacity in the coagulants extracted with saline solutions was higher, which reduces the required dosage for similar or superior performance [13,111].

The presence of organic residues in the extracted coagulant is undesirable because it promotes bacterial growth and serves as a substrate for by-product formation [113]. Therefore, the extracted natural coagulants must be purified. The most used purification method consists of removing the oil fraction in the coagulant extract through solvents, such as hexane and ethanol [111]. The decrease in lipid content enhances the removal of turbidity and COD, since oils hinder the coagulation process by adding impurities to the treated water [13]. Although this purification improves the performance of the natural coagulant, the extract can be further purified, yielding a final product with a high concentration of coagulation active compounds. To this end, several purification processes are being explored, such as chemical precipitation, dialysis, lyophilization, ultrafiltration, and ion exchange [95,105,112,116]. Sánchez-Martín et al. [112] investigated the effect of purification by ion exchange chromatography on the coagulation performance of moringa. The ideal coagulant dosage in a single elution step was twice that of the coagulant purified in two steps.

Due to the high cost of ion-exchange chromatography, researchers have been investigating alternative purification approaches [13]. An example is chemical precipitation with ammonium sulphate for extract purification [95,116]. Choudhary and Neogi [116] reported that moringa extract isolated with 30-60% and 60-80% saturated ammonium sulphate increased turbidity removal capacity compared to alum. This study suggests that a simple but effective purification method can produce natural coagulants with superior coagulation capacity.

Modification for improved performance

Natural coagulants exhibit certain limitations that can hinder their industrial application, including low solubility in water, undesirable isoelectric point, low stability (shelf life), narrow working window of pH range, weak surface charge, and moderate efficiency (translated to higher working dosage and cost) [70,131]. Reactive functional groups (e.g., hydroxyl, amino, and carboxyl) of natural coagulants promote modifications that can solve those concerns [13,76]. A study on the incorporation of valuable compounds through interaction with functional groups was carried out to remedy the negative points of natural coagulants. Generally, chemical reactions such as graft co-polymerization, crosslinking with aldehyde, esterification, etherification, amination, carboxyalkylation, hydroxyalkylation, and condensation have been adopted to improve the characteristics of natural coagulants [73].

Quarternized carboxymethyl chitosan is a modified chitosan used in coagulation processes. By including carboxymethyl and grafting of quarternary ammonium groups ((3-chloro-2-hydroxypropyl)-trimethylammonium chloride) onto the chitosan backbone, the isoelectric point of chitosan is dislocated from 6,0-6,5 to beyond pH 9, which expands the use for alkaline effluents and effluents [137]. Furthermore, the water solubility of modified chitosan is improved. The combination of improved water solubility, high isoelectric point, and more

positively charged functional groups enhances the performance of modified chitosan in removing contaminants compared to unmodified chitosan and synthetic coagulants.

Huang et al. [138] found that the positive charge of starch can be increased by introducing quaternary ammonium salt groups ((2-methacryloyloxyethyl) trimethylammonium chloride) onto the starch polymer backbone. A highly positive charge is desirable for coagulants because most suspended colloidal particles exhibit a negative surface charge. In the study by Huang et al. [138], a low dosage (0.5-0.7 ppm) of modified starch coagulant promoted removal rates as of 98%.

In addition to chemical modification and the search for efficient extraction and purification processes, natural coagulants can be combined with other coagulants (usually synthetic) [70,139]. More details on hybrid coagulants are presented in topic 3.4.

Multifunctional natural coagulants

As real effluents contain large amounts of impurities, various forms of treatment are necessary to remove the pollutants. The need for additional steps, sophisticated equipment, longer treatment time, and labor can increase the process costs [13]. Therefore, the use of multifunctional coagulants – capable of removing several types of pollutants in parallel – renders water and effluent treatment plants more compact and efficient [140].

The removal of suspended particles is the most common parameter to evaluate the performance of natural coagulants. However, the application of natural coagulants for the removal of pollutants such as heavy metals, organic compounds, and other contaminants should also be investigated. Typically, natural coagulants exhibit poor removal performance for dissolved contaminants [71,141]. Regardless of the coagulant used (natural or synthetic), coagulation has a low capacity to remove soluble heavy metals from effluents [70].

Consequently, coagulation must be integrated with other stages and unit operations to guarantee the complete removal of heavy metals and other dissolved pollutants [13,70].

To enhance the ability of the natural coagulant to remove multiple contaminants, functional groups with an affinity for such pollutants can be incorporated into the coagulant's molecular chain to produce modified coagulants. Yang et al. [142] introduced a dithiocarboxy group to the OH functional group on chitosan to produce xanthated chitosan. The researchers reported that copper (a heavy metal) and kaolin (responsible for turbidity) were successfully removed. Heavy metal chelating functional groups grafted onto natural coagulants allow the removal of coexisting copper, chromium, and nickel ions through the chelation process [143].

Viability of natural coagulants

Natural coagulants (modified, unmodified or hybrid) that demonstrate promising performance in laboratory tests should be scaled up to pilot and industrial-scale applications. The industrial viability of natural coagulants as to their performance, costs, and technical aspects should also be further investigated. Furthermore, the potential of plant-based coagulants in rural and impoverished areas should be explored, as natural coagulants can be locally sourced. Moreover, quality control tools can be used to standardize and optimize production [13,18,77].

Sustainability of natural coagulants

The investigation of sustainability criteria (environmental, economic, and social) will help elucidate uncertainties about natural coagulants. A constant supply of raw materials for the extraction and synthesis of natural coagulants might be necessary to ensure competition with conventional coagulants. A comprehensive cost study is needed to define the economic viability of natural coagulants, comprising the cost of raw materials, extraction, and purification.

Investigating the health and environmental impacts of natural coagulants (especially modified natural coagulants) can provide relevant results. In addition, a life cycle assessment may indicate opportunities for improvement in the coagulation process with natural agents. Finally, an analysis based on circular economy and bioeconomy concepts can contribute to the development and sustainability of natural coagulants used to treat effluents [13,18,74,77].

10. CONCLUSIONS

Despite the encouraging results reported on plant-based coagulants to treat food industry effluents, the number of information gaps identified in this research field is significant. For instance, only a few studies have elucidated the underlying coagulation mechanisms of natural coagulants, while the analysis of the coagulation efficiency of different plant-based materials for various types of effluents and coagulant combinations is still in its infancy. Studies reporting the economic aspects are exceptionally scarce. Despite the opportunities for improvement, the current scientific literature reports vital results:

- Plant-based coagulants are efficient for turbidity and pollutant removal;
- Although purification is not mandatory, it is frequently used to prevent an increase in organic matter concentration after the effluents treatment;
- High cost-efficiency and low toxicity are among the fundamental advantages of plant-based coagulants, both as sole coagulants and coagulation aid;
- The utilization of natural coagulants to treat food industry effluents has been limited to academic research. These studies must be scaled-up given the high potential of natural coagulants in sustainable environmental technologies;

- Among the factors hindering further use of natural coagulants are the limited cultivation of plants with coagulant properties and the lack of regulation specifying the quality of processed coagulant extracts;
- *M. oleifera* is the most researched source of plant-based coagulants. The results summarized herein for moringa can be employed to optimize process conditions for this species or can be used as a starting point for the investigation of other plant species.

The industrial acceptance of natural coagulants over conventional coagulants is still negligible. We trust this review paper will contribute to a more widespread application of natural coagulants by showcasing their properties.

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Table 1 – Operational conditions used in the treatment of food industry effluents with plant-based coagulants.

Wastewater	Coagulant	Process temperature (°C)	Coagulant dosage	Effluent volume (L)	pH	Equipment	Coagulation	Flocculation	Sedimentation	Main findings	Reference
							Fast mixing	Slow mixing			
Dairy industry	<i>Moringa oleifera</i> seeds	25±1	0.15–0.25 g	0.2	5–10	Jar-Test	Different rotational speeds for up to 60 min		60 min	Up to 98% removal of color and turbidity.	[9]
Dairy industry	<i>Moringa oleifera</i> seeds	-	0.5–1.25 g/L	-	-	Jar-Test	200 rpm for 1 min	100 rpm for 40 min	40–60 min	Over 95% turbidity removal.	[28]
Dairy industry	<i>Moringa oleifera</i> seeds	-	100–400 mg/L	-	-	Jar-Test	60 s	15–20 rpm	30 min	Mean removal efficiency of 62.5% for turbidity, 51.9% for COD, and 80% for salinity.	[29]
Dairy industry	Vegetable tannin	-	100–600 mg/L	1.5	6.0–7.0	Jar-Test	120 rpm for 90 s	45 rpm for 30 min	60 min	48.1- 78.5% color removal at concentration 100-600 mg/L; maximum TS removal of 13.6% at 500 mg/L; maximum COD removal of 41.6% at 400 mg/L; maximum turbidity removal of 89.4% at 300 mg/L.	[30]
Dairy industry	<i>Moringa oleifera</i> seeds	-	3000 mg/L	-	no pH correction	Jar-Test	100 rpm for 2 min	20 rpm for 10 min	60 min	Removal efficiency of 96-99% for COD, turbidity, and color.	[31]
Dairy industry cleaning-in-place	Moringa seed extract and nanoparticles of iron oxide functionalized with moringa extract	-	800–2000 mg/L	0.25	natural pH and 9	-	100 rpm for 2 min	20 rpm for 10 min	60 min	Nearly 90% turbidity removal.	[32]

Dairy cattle breeding	<i>Moringa oleifera</i> seeds	-	60 mL	1	7.2	Organic filters made of thin coal, bamboo leaves, eucalyptus leaves, gliricidia branches, and wood sawdust	Manual stirring for 10 min		-	Removal efficiency up to 44.60% for TS, 49.23% for TSS, and 43.38% for COD.	[33]
Palm oil milling	<i>Cassia obtusifolia</i> seeds	20–90	0–2.5 g/L	0.3	2–4.7	Jar-Test	150 rpm for 5 min	0–50 rpm for 15 min	0–60 min	Maximum removal of 81-87% for TSS and 48-55% for COD.	[6,7]
Palm oil milling	<i>Moringa oleifera</i> seeds	50–70	500–6000 mg/L and 1000–5000 mg/L	0.5	4–9 and 3–7	Jar-Test	150 rpm for 5 min	30 rpm for 30 min	90 min	Removal efficiency up to 99.7% for TSS, 71.5% for COD, 68.2% for BOD, 100% for oil and grease, and 91% for total nitrogen.	[34–36]
Palm oil milling	Rice starch	25±1	0–3.0 g/L	0.3	2.5–9	Conventional jar or flocculator	150 rpm for 5 min	0–100 rpm for 15 min	0–90min	TSS removal up to 84.1% for rice starch alone and 88.4% for rice starch and 0.20-0.8 g/L of alum. COD removal up to 49.23% using rice starch and 0.38 g/L alum.	[37,38]
Palm oil milling	Magnetic <i>Moringa oleifera</i> seeds	-	0.5–2.5 g/L	1	5–9	Jar-Test	150 rpm for 2 min	30 rpm for 30 min	1–45 min	Approximately 90% COD removal.	[39]
Palm oil milling	<i>Moringa oleifera</i> seeds	27–30	500–5000 mg/L	0.5	4.51	Jar-Test	250 rpm and 3 min	30 rpm and 30 min	60 min	The optimal moringa dosage (2000 mg/L) provided removal	[40]

										percentages of 95.42% for TSS, 88.30% for turbidity, 90.15% for color, 89.81% for NH ₃ -N, and 87.05% for oil and grease.	
Cassava processing	<i>Abelmoschus esculentus</i> (Okra), <i>Ficus exasperata</i> (Ipil tree), and <i>Bridelia ferrugineae</i> (Iraodan tree)	-	0–100 mL	0.25	-	Jar-Test	30 s at 120 rpm	20 rpm for 15 min	60 min	Turbidity was reduced from 168 NTU to as low as 6 NTU.	[41]
Cassava processing	Natural commercial coagulants (Acquapol WW, Acquapol S5T, Tanfloc SL, and Tanfloc SG)	-	160–800 mg/L	0.5	natural pH	Jar-Test	120 rpm for 2 min	20 rpm for 15 min	5–20 min	Removal efficiency over 77.5% for color and 88.5% for turbidity.	[42]
Tapioca starch	<i>Moringa oleifera</i> seeds	26	110–150 mg/L	1	-	Clarifier tank	15–20 rpm for 5 min		3 h	Up to 99.6% removal for BOD, 99.7% for COD, and 91.5% for TSS. The effluent's pH increased from 5.8 to 6.7–7.8.	[8]
Coffee fruit pulping	<i>Moringa oleifera</i> seeds	25	0–60 mL/L	-	4–8	Jar-Test	160 rpm for 10 s	20 rpm for 5 min	90 min	Up to 84.27% TSS removal.	[43]

Coffee fermentation	<i>Moringa oleifera</i> seeds	-	0–4 g/L	0.9	3–7	Jar-Test	2 min	5 min	24 h	Up to 54% removal efficiency for TSS, 100% for insoluble COD, 25% for total COD, and 100% for nitrates and nitrites.	[44]
Distillery spent wash	<i>Moringa oleifera</i> seeds	30	20–60 mL	0.5	4–9	Jar-Test	100 rpm for 2 min	40 rpm for 30 min	30 min	Maximum 56% and 67% color removal using moringa coagulant along with sodium chloride and potassium chloride, respectively.	[45]
Distillery spent wash	<i>Moringa oleifera</i> seeds	30	20–80 mL/L	1	2–6	Jar-Test	300 rpm for 2 min	30 rpm for 30 min	4 h	Removal efficiencies varied depending on the synthetic coagulants (ferric sulphate, aluminium sulphate, and calcium sulphate) used in conjunction with moringa. Aluminium sulphate along with moringa extract at pH 4.0 yielded the best removal rates: 97% for color, 87% for COD, and 100% for turbidity.	[46]
Swine farms	<i>Moringa oleifera</i> seeds	-	1–20 mL	0.5	4.2	Jar-Test	160 rpm for 30 s	15 rpm for 15 min	2–24 h	Total and thermotolerant coliforms were reduced by 96.5% and 94.8%, respectively, but turbidity was not affected.	[47]
Brewery	Vegetable tannin	25	0.12–0.18 mL/L	1.2	4.5–8	Jar-Test	120 rpm for 5 min	30 rpm for 30 min	10 min	99% turbidity removal.	[25]

Green tea extracts	<i>Moringa oleifera</i> seeds	-	100–10000 mg/L	-		Jar-Test	150 rpm for 5 min	30 rpm for 30 min	-	Removal of turbidity, TS, and polyphenols up to 96%, 16%, and 19%, respectively.	[48]
Slaughterhouse	<i>Moringa oleifera</i> seeds	25±1	3–7 g/L	1	5–9	Jar-Test	100 rpm for 5 min	20 rpm for 20 min	180 min	Up to 64% COD reduction.	[4]

Abbreviations: BOD = biochemical oxygen demand; COD = chemical oxygen demand; NH₃-N = ammonia nitrogen; TS = total solids; TSS = total suspended solids.

Table 2 – Use of plant-based coagulants in the treatment of food industry effluents.

Coagulant source	Effluent	Objectives	Main results	Reference
<i>Moringa oleifera</i> seeds	Dairy industry wastewater	Investigate the sorption potential of moringa seeds in the removal of organic compounds from wastewater	Removal efficiencies of up to 98% for both color and turbidity using 0.2 g of moringa seed powder	[9]
<i>Moringa oleifera</i> seeds	Slaughterhouse wastewater	Investigate the adsorption of organic pollutants when moringa seed is employed as a natural coagulant	64% COD reduction using 7 g/L of powdered seed and pH 9	[4]
<i>Cassia obtusifolia</i> seeds	Palm oil mill effluent	Evaluate the potential of cassia seed gum as a natural coagulant alternative to alum	<i>C. obtusifolia</i> seed gum is as efficient to treat palm oil mill effluent as alum: at least 87% removal of TSS and 55% COD at concentration 1.0 g/L, initial wastewater pH 3, and settling time 45 min	[6]
<i>Moringa oleifera</i> seeds	Tapioca starch wastewater	Investigate the addition of powdered moringa seed in reducing physicochemical parameters and total coliform, as well as increasing pH	BOD, COD, and TSS were significantly reduced, while pH reached the acceptable range for effluent disposal	[8]
<i>Moringa oleifera</i> seeds	Coffee fruit pulping wastewater	Determine the best combination between pH and concentration of moringa seed extract	Greater removal of suspended solids from the wastewater at pH 4.0-5.0 and dosage 10 mL/L	[43]

<i>Moringa oleifera</i> seeds	Coffee fermentation wastewater	Investigate the efficacy of moringa seed extract in wastewater treatment	Significant reduction of TSS (from 8% to 54%), COD (from 26% to 100%), and nitrate and nitrite (from 20% to 100%)	[44]
<i>Moringa oleifera</i> seeds	Palm oil mill effluent	Evaluate the use of moringa seeds as natural coagulant in the coagulation-flocculation of effluent	95% removal of suspended solids and 52.2% reduction of COD, with best performance at 30°C	[34]
<i>Moringa oleifera</i> seeds	Distillery spent wash	Determine the effects of moringa-based coagulant dosage, pH, and salt concentration in effluent color removal	Partial color removal was obtained at optimal conditions, which were selected through the response surface methodology	[45]
<i>Moringa oleifera</i> seeds	Distillery spent wash	Evaluate the efficiency of moringa seed extract along with conventional coagulants for the removal of physical-chemical contaminants from effluent	Moringa seed extract exhibited significant color, COD, and turbidity reduction ability when used as a coagulant aid along with synthetic coagulants. Aluminum sulphate combined with moringa seed extract was most effective, removing 96.5% of color, 87% of COD, and 99.9% of turbidity at pH 4.0	[46]
<i>Moringa oleifera</i> seeds	Porcine wastewater	Evaluate the efficiency of moringa seed extract in the removal of turbidity and coliforms (total and thermotolerant) from wastewater	Turbidity remained unchanged, but total and thermotolerant coliforms were removed by 96.5% and 94.8%, respectively	[47]

<i>Moringa oleifera</i> seeds	Dairy cattle breeding wastewater	Evaluate the effect of moringa extract on the removal of TS, TSS, and COD from wastewater	Moringa seed extract increased the efficiency of organic filters in TS and COD removal, but TSS removal efficiency remained unchanged	[33]
<i>Moringa oleifera</i> seeds	Dairy industry wastewater	Evaluate the environmental and economic potential of the application of moringa seed powder in wastewater treatment	Turbidity was reduced by over 95%, enabling water reuse. The cultivation of moringa can be an extra source of revenue for dairy farmers	[28]
<i>Moringa oleifera</i> seeds	Dairy industry wastewater	Study moringa seed powder as a natural adsorbent for wastewater treatment	Successful removal of turbidity, COD, and salinity	[29]
Vegetable tannins	Brewery wastewater	Evaluate and optimize coagulation-flocculation conditions	99% removal of turbidity and reduction of apparent color using 0.23 mL/L of vegetable tannin at pH 4.9. Tanfloc SL aided flocculation, enabling water reuse	[25]
<i>Moringa oleifera</i> seeds	Green tea extracts	Compare the isolated effect of centrifugation to the impact of natural coagulants (chitosan and moringa) followed by centrifugation in green tea extract clarification	Optimized clarification conditions provided turbidity, TS, and polyphenols reductions of 96%, 16%, and 19% using moringa extract versus 95%, 16%, and 18% using chitosan. The extraction and clarification with moringa followed by centrifugation produced clear green tea extracts enriched with bioactive compounds at a lower cost	[48]
Rice starch	Palm oil mill effluent	Evaluate the performance of unmodified starches as natural	Rice starch and alum yielded similar TSS removal at dosage 2 g/L, pH 3, settling time 5 min, and stirring rate 10 rpm	[37]

		coagulants in coagulation-flocculation treatment compared to alum coagulant		
<i>Moringa oleifera</i> seeds	Dairy wastewater	Evaluate the use of moringa as a natural coagulant in CFS followed by MF or NF in wastewater treatment	The association of CFS-MF-NF treatments showed removal efficiencies between 96% and 99% for COD, turbidity, and color, meeting water reuse standards. The treated wastewater exhibited better quality compared to the conventional method	[31]
<i>Abelmoschus esculentus</i> (Okra) pods, <i>Ficus exasperata</i> (Ipin tree) bark, and <i>Bridelia ferrugineae</i> (Iraodan tree) bark	Cassava processing	Determine the coagulant efficiency of three organic coagulants compared to an synthetic coagulant (aluminum sulphate)	For wastewater with initial turbidity of 168 NTU, the lowest turbidity attained upon applying the three organic coagulants was 6 NTU. The organic coagulants employed can partially replace the synthetic coagulant	[41]
<i>Moringa oleifera</i> seeds	Palm oil wastewater	Determine the COD removal efficiency of magnetic moringa obtained from moringa seeds and synthetic magnetic nanoparticles	The microwave synthesis of magnetic moringa is a cost-efficient process in the production of a highly effective coagulant (90% COD removal)	[39]
<i>Moringa oleifera</i> seeds	Palm oil mill effluent	Determine the optimum coagulant dose for contaminant removal	The optimum dosage was 2000 mg of powdered seeds per L of effluent	[40]
Vegetable tannins	Dairy wastewater	Compare the coagulation performance of tannin and polyaluminum chloride	No statistical differences between the performance of the two coagulants for the removal of COD, color, turbidity, and TS. Tannins were effective within a wide pH range (5.0 to 10.0)	[30]

Natural commercial coagulants (Acquapol WW, Acquapol S5T, Tanfloc SL, and Tanfloc SG)	Cassava processing wastewater	Investigate the efficiency of different coagulants in color and turbidity removal from effluent	Natural commercial coagulants yielded a higher color and turbidity removal than the synthetic coagulant. The best concentration of natural coagulant (Acquapol S5T and Tanfloc SL) was 320 mg/l, removing color by $\geq 77.5\%$ and turbidity by $\geq 88.5\%$	[42]
<i>Moringa oleifera</i> seeds extract and nanoparticles of iron oxide functionalized with moringa extract	Dairy cleaning-in-place wastewater	Test two organic coagulants derived from moringa as alternatives for wastewater treatment	Mo-NP provides approximately 90% of turbidity removal in a reduced sedimentation time (7 min compared to 60 min when Mo is used alone)	[32]

Abbreviations: BOD = biochemical oxygen demand; CFS = coagulation/flocculation/sedimentation; COD = chemical oxygen demand; MF = microfiltration; Mo = moringa seeds extract; NF = nanofiltration; NP = nanoparticles; TS = total solids; TSS = total suspended solids

Table 3 – Natural coagulants used in the treatment of food industry effluents.

Effluent	Coagulant source	Coagulant preparation	Reference
Dairy industry wastewater	<i>Moringa oleifera</i> seeds	The biomass was cut, ground, and sieved. Then, the fraction with a mesh size <0.42 mm was selected. The seeds did not undergo drying or any other processing.	[9]
Slaughterhouse wastewater	<i>Moringa oleifera</i> seeds	The seeds were shelled, reduced to a fine powder, and sieved. White seed kernels with mesh size 0.51 mm were selected.	[4]
Palm oil mill effluent	<i>Cassia obtusifolia</i> seeds	Whole seeds were ground (0.5-1 mm), and 2.5 g samples were mixed with 100 mL of distilled water for 30 s. The mixture was filtered and the filtrate was used as gum.	[6,7]
Tapioca starch wastewater	<i>Moringa oleifera</i> seeds	Seeds were peeled, dried, and milled. Fine powders that passed through a 50-mesh sieve were used as a coagulant.	[8]
Coffee fruit pulping wastewater	<i>Moringa oleifera</i> seeds	The extract was obtained by mixing macerated seeds with water (10 mL of water for each seed).	[43]
Coffee fermentation wastewater	<i>Moringa oleifera</i> seeds	0.1 g of ground seeds were mixed with 25 mL of distilled water for 1 min before filtering the resulting solution.	[44]
Palm oil mill effluent	<i>Moringa oleifera</i> seeds	Seeds were ground to a fine powder, and the oil was extracted for 8 h with n-hexane. After drying the resulting cake, 5 g were mixed with 100 mL distilled water for 2 min. The resulting suspension was filtered.	[34–36]
Distillery spent wash	<i>Moringa oleifera</i> seeds	The seeds were ground to a fine powder, and the active component was extracted using 100 mL of NaCl or KCl solution for each 4 g of powder. The mixture was stirred for 30 min at room temperature, and the suspension was filtered.	[45]

Distillery spent wash	<i>Moringa oleifera</i> seeds	The active components from the seeds were extracted using 100 mL of 1 M NaCl solution for each 5 g of powdered seed mixed at 500 rpm for 15 min at room temperature. Then, the coagulant salt suspension was filtered.	[46]
Porcine wastewater	<i>Moringa oleifera</i> seeds	1 g, 2 g, and 3 g samples of ground seeds were extracted with 100 mL of distilled water. The mixture was then filtered.	[47]
Dairy cattle breeding	<i>Moringa oleifera</i> seeds	Seeds were removed from the pods and dried in an oven at 45 °C for 24 h. The moringa extract was prepared by grinding 50 g of seeds in 1 L of distilled water followed by filtration.	[33]
Dairy industry wastewater	<i>Moringa oleifera</i> seeds	Two methods were employed: (1) 2 g of ground seeds were extracted with 1 mol/L NaCl solution (11.89 g in 200 mL water); and (2) seed pods were peeled and crushed, and the resulting powder was sieved through a 42 mm sieve.	[28]
Dairy industry wastewater	<i>Moringa oleifera</i> seeds	2 g of dried and finely ground seeds were extracted with 100 mL water. The suspension was stirred for 30 min and then passed through a filter paper.	[29]
Brewery wastewater	Vegetable tannin from <i>Acacia mearnsii</i>	Tanfloc was used as a flocculant. This is a commercial vegetable tannin derived from the leaching of black acacia bark.	[25]
Green tea extracts	<i>Moringa oleifera</i> seeds	Peeled and ground seeds were Soxhlet-extracted with 98% purity n-hexane for 8 h. After removal of the oil fraction, the powdered seeds were mixed with water at a ratio of 20 mL/g, and the mixture was filtered with an 11 µm paper filter.	[48]
Palm oil mill effluent	Rice starch	6 g of starch were added to 200 mL of distilled water. This mixture was firstly autoclaved at 121 °C and 117 kPa for 20 min, and then kept at a constant temperature of 80 °C with an agitation of 400 rpm.	[37,38]

Dairy wastewater	<i>Moringa oleifera</i> seeds	The coagulant solution was prepared by mixing 50 g of ground seeds with 1 L of 1 M potassium chloride solution. The mixture was stirred for 30 min and the solution was vacuum filtered.	[31]
Cassava processing wastewater	<i>Abelmoschus esculentus</i> (Okra), <i>Ficus exasperata</i> (Ipin tree), and <i>Bridelia ferrugineae</i> (Iraodan tree)	Okra: pods were ground to produce the gum, and 1.0 g of gum was soaked in 100.0 mL of water under stirring for 1 h. The mucilage used as coagulant was thereafter obtained by filtering the resulting solution. Ipin tree and Iraodan tree: 200 g of the barks of both plants were soaked in 2 L of water for 3 days.	[41]
Palm oil wastewater	Magnetic <i>Moringa oleifera</i>	3 g of seed powder were mixed with 0.1 L of 0.5 M calcium chloride under 100 °C for 30 min at 100 rpm. Then, the extracted solution was microwaved and sonicated. The microwave power and ultrasonic intensity varied within 200 to 800 W and 20 to 100%, respectively. The mixture was filtered and oven-dried at 60 °C.	[39]
Dairy wastewater	Vegetable tannin from <i>Acacia mearnsii</i>	Tannin based coagulant was extracted from <i>Acacia mearnsii</i> (TANAC, 25% w/w concentration).	[30]
Cassava processing wastewater	Natural commercial coagulants from <i>Acacia mearnsii</i>	Several commercial natural coagulants extracted from the husk of <i>Acacia-negra</i> were tested, namely: Acquapol WW and Acquapol S5T (Acqua Química), and Tanfloc SL and Tanfloc SG (Tanac S.A). The Tanfloc SL and SG solutions were prepared by dissolving 2 g of coagulant in 50 mL water. Solutions of Acquapol WW and S5T coagulants consisted of 5 mL of coagulant for every 50 mL of water.	[42]
Dairy cleaning-in-place wastewater	Moringa seeds extract and nanoparticles of iron oxide functionalized with moringa extract	Extract: moringa coagulant was prepared by grinding 5 g of shelled seeds in a mill and then stirring this powder with 100 mL of a saline solution for 30 min. Then, the coagulant was obtained by vacuum filtering the extract.	[32]

		Magnetic coagulant: predetermined quantities of nanoparticles (50 or 100 mg) were added to 20 mL of moringa extract and sonicated for 5 min followed by 1 h of stirring.	
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Methodology employed





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Plant-based coagulants for food industry wastewater treatment

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ABSTRACT

Sustainable effluent treatments are essential tools in lowering the environmental impact of industrial activities. The partial or complete replacement of synthetic coagulants by natural coagulants, especially plant-based ones, can reduce the footprint of the effluent treatment due to the higher biodegradability and non-toxicity. Natural coagulants are also generally cheaper. This review focuses on plant-based coagulants used in food industry wastewater treatment. Extraction parameters of plant-based coagulants and effluent treatment conditions for different coagulants are presented. Based on an extensive assessment of peer-reviewed papers on food industry wastewater treatment, the performance of plant-based coagulants is compared to that of traditional, synthetic coagulants, both alone and as coagulant aids. This review aims to guide researchers and industry professionals in optimizing and scaling up environment-friendlier wastewater treatments using natural coagulants.

1. Introduction

Industrial activities are one of the leading causes of water pollution due to the generation of significant amounts of wastewater that contain toxic species or species that are difficult to degrade [1]. The production of liquid waste by the food industry is sizeable, especially in the animal-based food sector. Slaughtering operations and meat processing generate massive volumes of wastewater rich in proteins, organic compounds, and fats [5]. For example, slaughtering a single pig or cow generates 330 L and 700 L of wastewater, respectively [2–4]. Although drastically less than the animal sector, the production of plant-derived foods also uses significant amounts of water. For instance, the production of one ton of crude palm oil requires 5–7.5 tons of water [6,7]. Another example is the cassava starch industry, which generates 12–15 L of wastewater for each m³ of processed cassava. The wastewater from cassava starch production exhibits high biochemical oxygen demand (BOD), chemical oxygen demand (COD), total suspended solids (TSS),

total solids (TS), and cyanides [8].

Inadequate disposal of food industry effluents impacts the environment due to the high load of organic matter, heavy metals, alkalinity, and hardness, resulting in water pollution, odor generation, algal blooms, and mortality of aquatic and land animals [4,9]. The appropriate treatment of industrial wastewater is carried out by Effluent Treatment Stations (ETs) [10]. By diminishing the polluting load of effluents, ETs enable their safe reuse or release into water bodies.

To treat wastewater, ETs utilize coagulation, flocculation, sedimentation, and other physical, chemical, and biological processes [11]. Wastewater treatments can be classified into physical (media filtration, settling, adsorption, membrane, and ultraviolet radiation), chemical (electrochemical, coagulation, oxidation, ion exchange, disinfection, catalytic reduction, and softening), and biological (microbial biodegradation, phytoremediation, constructed wetlands, and bioreactor digestion) [12,13]. Among these technologies, coagulation, and flocculation (CF) are the oldest and most widely employed in wastewater

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